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(54) **GASIFICATION SYSTEM EMPLOYING  
EJECTORS**

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**C10K 1/10** (2006.01)  
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**C10K 1/10** (2013.01); **C02F 2103/365**  
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B01D 3/105; B01D 3/106; B01D 3/108  
See application file for complete search history.

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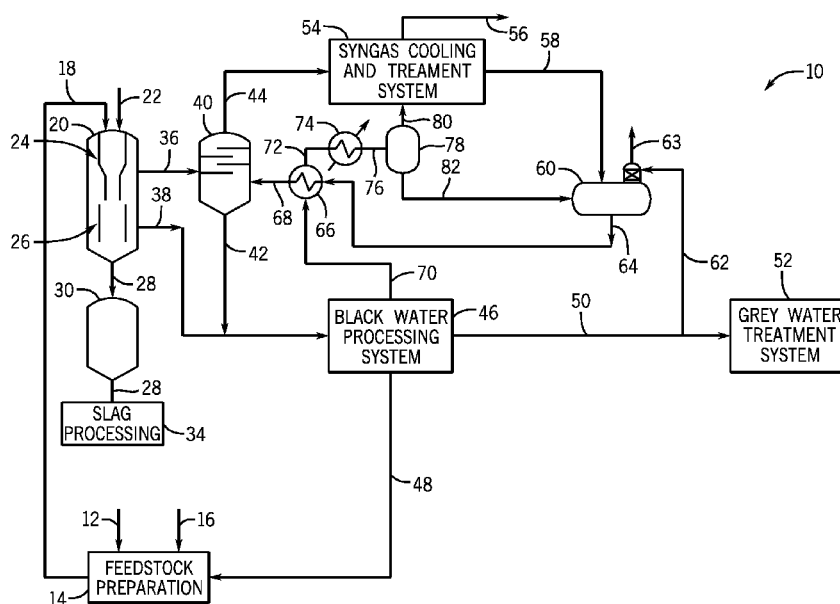
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(57) **ABSTRACT**

In one embodiment, a black water processing system includes a vacuum pressure flash tank configured to separate gases from black water. The system also includes an ejector with a suction chamber and a nozzle. The suction chamber is coupled to the vacuum pressure flash tank, and the nozzle is configured to discharge a motive fluid across the suction chamber to create a vacuum within the vacuum pressure flash tank.

**19 Claims, 3 Drawing Sheets**



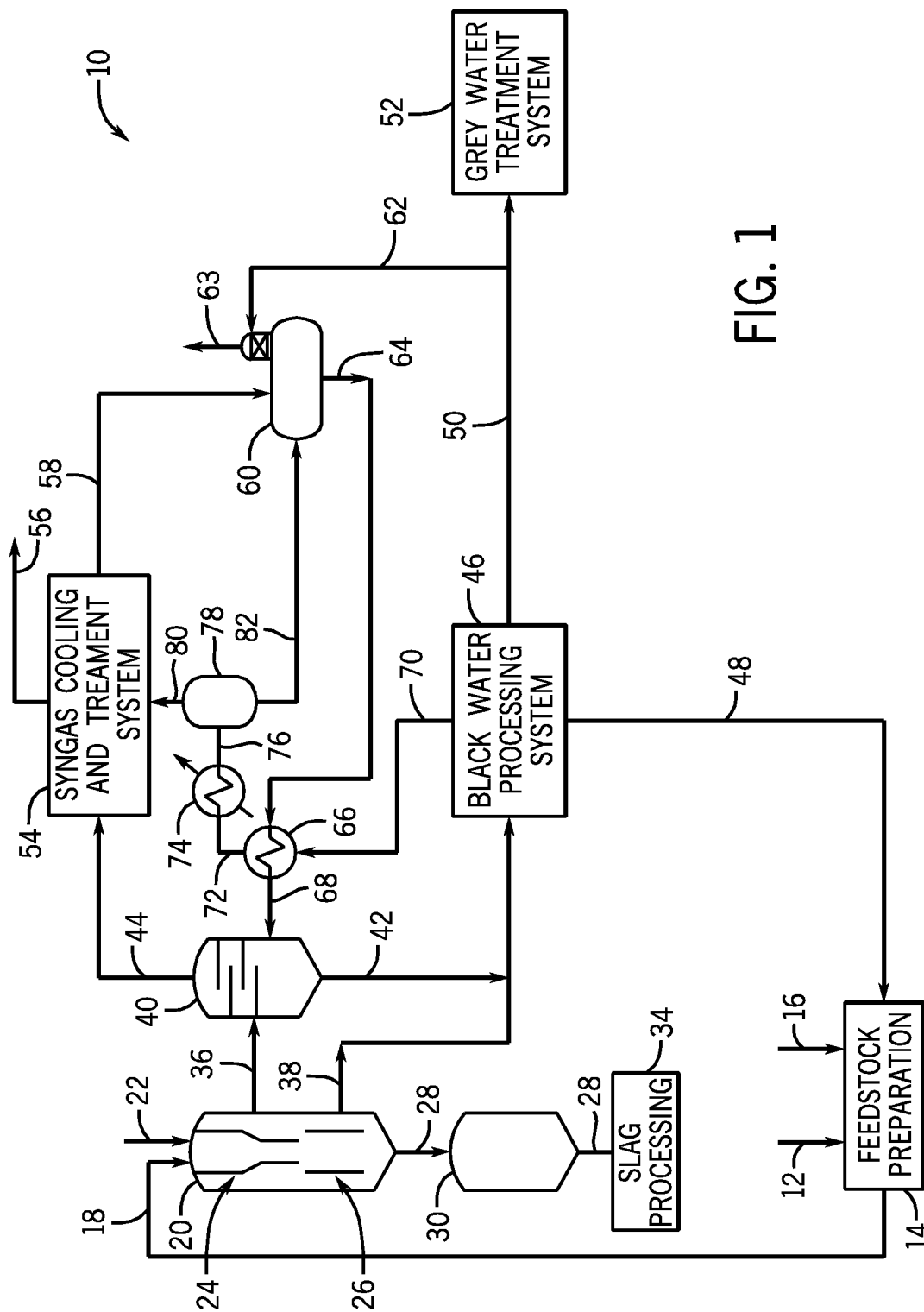


FIG. 1

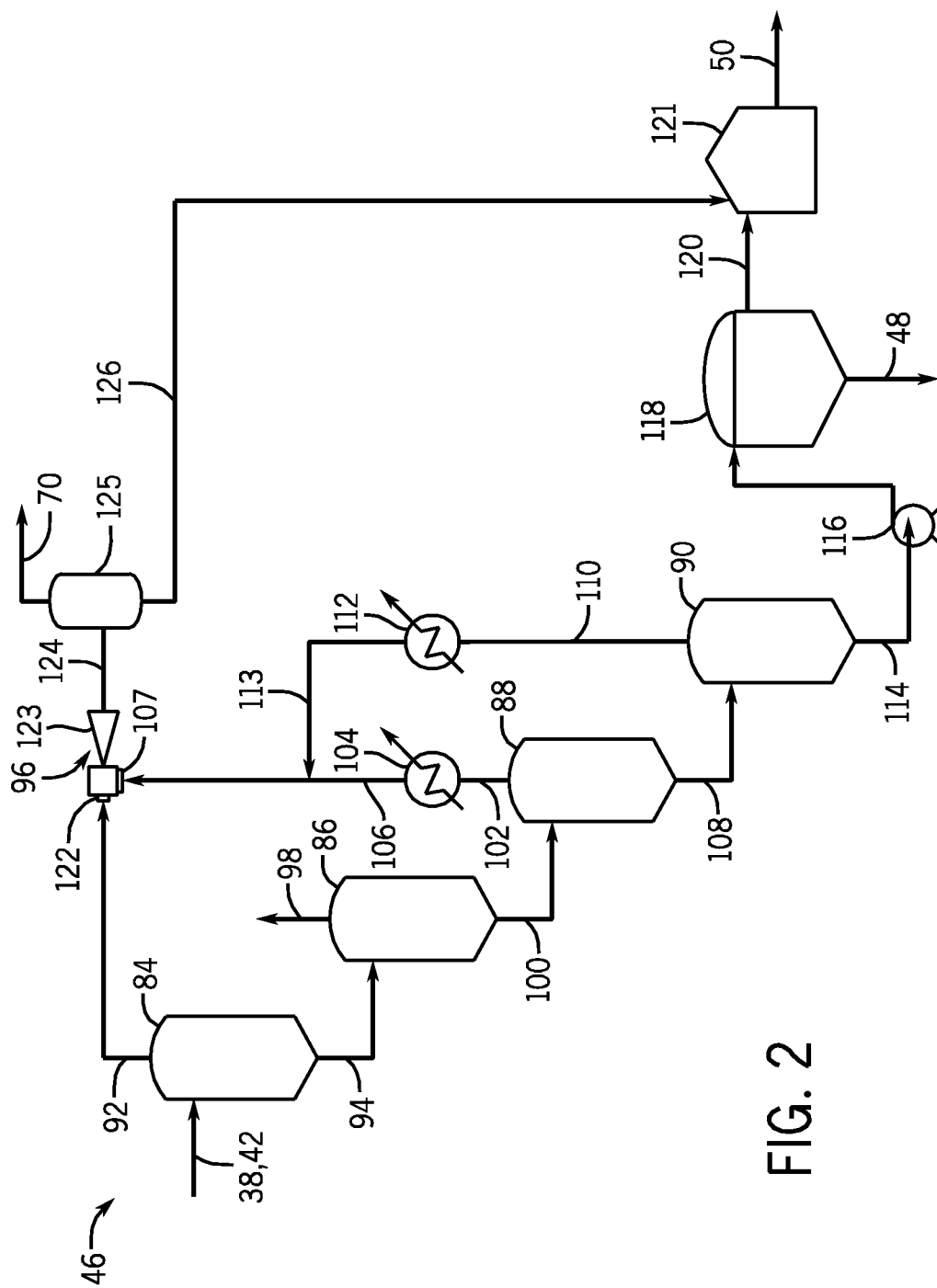


FIG. 2

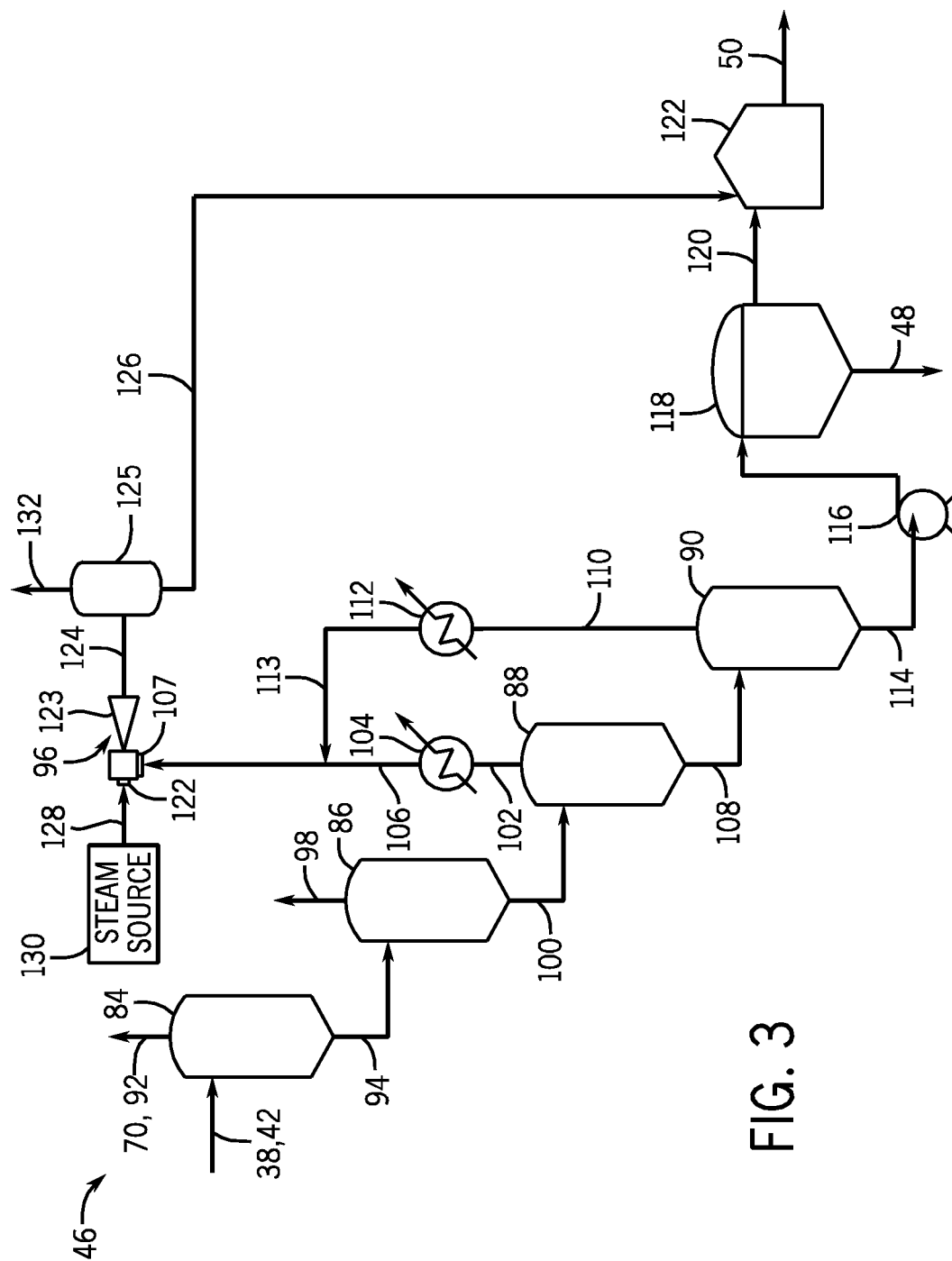


FIG. 3

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## GASIFICATION SYSTEM EMPLOYING EJECTORS

### BACKGROUND OF THE INVENTION

The subject matter disclosed herein relates to gasification systems employing ejectors, and more particularly, to black water processing systems employing ejectors.

Fossil fuels, such as coal or petroleum, may be gasified for use in the production of electricity, chemicals, synthetic fuels, or for a variety of other applications. Gasification involves reacting a carbonaceous fuel and oxygen at a very high temperature to produce syngas, a fuel containing carbon monoxide and hydrogen, which burns more efficiently and cleaner than the fuel in its original state. A byproduct of gasification is black water, which may include particles of ash, metals, ammonia, and organic matter as well as dissolved gases.

### BRIEF DESCRIPTION OF THE INVENTION

Certain embodiments commensurate in scope with the originally claimed invention are summarized below. These embodiments are not intended to limit the scope of the claimed invention, but rather these embodiments are intended only to provide a brief summary of possible forms of the invention. Indeed, the invention may encompass a variety of forms that may be similar to or different from the embodiments set forth below.

In a first embodiment, a black water processing system includes a vacuum pressure flash tank configured to separate gases from black water and an ejector with a suction chamber and a nozzle. The suction chamber is coupled to the vacuum pressure flash tank, and the nozzle is configured to discharge a motive fluid across the suction chamber to create a vacuum within the vacuum pressure flash tank.

In a second embodiment, a gasification system includes a high-pressure flash tank configured to separate gases from black water to produce a first discharge of the black water and a second discharge of separated gases. The gasification system also includes an ejector with a suction chamber and a nozzle. The nozzle is configured to discharge the second discharge across the suction chamber to create a vacuum.

In a third embodiment, a gasification system includes a gasifier configured to produce a synthetic gas and black water and a black water processing system. The black water processing system includes a high-pressure flash tank configured to flash the black water to produce a first vapor discharge of first separated gases and a first liquid discharge of the black water, and a vacuum pressure flash tank configured to flash the black water to produce a second vapor discharge of second separated gases and a second liquid discharge of the black water. The gasification system also includes an ejector with a suction chamber and a nozzle. The suction chamber is coupled to the vacuum pressure flash tank, and the nozzle is configured to discharge the first vapor discharge across the suction chamber to pull the second vapor discharge into the ejector from the vacuum pressure flash tank.

### BRIEF DESCRIPTION OF THE DRAWINGS

These and other features, aspects, and advantages of the present invention will become better understood when the following detailed description is read with reference to the accompanying drawings in which like characters represent like parts throughout the drawings, wherein:

FIG. 1 is a schematic block diagram of an embodiment of a gasification system;

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FIG. 2 is a schematic block diagram of an embodiment of the black water processing system of FIG. 1; and

FIG. 3 is a schematic block diagram of another embodiment of the black water processing system of FIG. 1.

### DETAILED DESCRIPTION OF THE INVENTION

One or more specific embodiments of the present invention will be described below. In an effort to provide a concise description of these embodiments, all features of an actual implementation may not be described in the specification. It should be appreciated that in the development of any such actual implementation, as in any engineering or design project, numerous implementation-specific decisions must be made to achieve the developers' specific goals, such as compliance with system-related and business-related constraints, which may vary from one implementation to another. Moreover, it should be appreciated that such a development effort might be complex and time consuming, but would nevertheless be a routine undertaking of design, fabrication, and manufacture for those of ordinary skill having the benefit of this disclosure.

When introducing elements of various embodiments of the present invention, the articles "a," "an," "the," and "said" are intended to mean that there are one or more of the elements. The terms "comprising," "including," and "having" are intended to be inclusive and mean that there may be additional elements other than the listed elements.

The present disclosure is directed to gasification systems that employ ejectors to create a vacuum. In addition to producing syngas, gasification systems may produce black water that contains fine particles of ash, ammonia, metals, and organic material, as well as dissolved gases. Black water generally includes quench and/or scrubbing water that contains a relatively large amount of carbon containing solids. The black water may be processed through a series of flash tanks to separate the dissolved gases from the black water and produce black water concentrated with the fine particle solids. The series of flash tanks may include one or more high-pressure flash tanks, intermediate and/or low-pressure flash tanks, and vacuum flash tanks, with each flash tank in series having a progressively lower pressure to separate additional dissolved gases from the black water.

As disclosed herein, a vacuum may be created within the vacuum flash tanks through the use of an ejector. An ejector may generally include a nozzle that discharges a high-velocity jet across a suction chamber connected to a piece of equipment, such as a tank, that is to be evacuated. In particular, a suction chamber of the ejector may be coupled to the vacuum flash tanks and a high-pressure motive fluid may be discharged at a high velocity across the suction chamber to create a vacuum within the vacuum flash tanks. The ejector includes only stationary parts and therefore contains no moving parts, which may reduce capital and/or operating costs when compared to the use of a traditional liquid ring vacuum pump, which requires moving parts as well as a power supply and a water supply. The motive fluid used in the ejector may be steam or another high-pressure fluid. According to certain embodiments, the overhead discharge of separated gases from the high-pressure flash tank may be used as the motive fluid in the ejector.

FIG. 1 illustrates a gasification system 10 that may employ one or more ejectors. Within the gasification system 10, a carbonaceous fuel source 12 may be utilized as a source of energy to produce syngas. The fuel source 12 may include

coal, petroleum coke, biomass, wood-based materials, agricultural wastes, tars, coke oven gas and asphalt, or other carbon containing materials.

The fuel source **12** may be introduced into the gasification system **10** via a feedstock preparation system **14**. The feedstock preparation system **14** may resize or reshape the fuel source **12**, for example, by chopping, milling, shredding, pulverizing, briquetting, or palletizing the fuel source **12** to create a fuel slurry **18**. According to certain embodiments, the feedstock preparation system **14** may include a grinding mill. Further, within the feedstock preparation system **14**, additives, **16**, such as water, or other suitable liquids, may be added to the fuel source **12** to create the fuel slurry **18**. However, in other embodiments, where no liquid additives are employed, the fuel slurry **18** may be a dry feedstock.

The fuel slurry **18** may be directed to a gasifier **20** where the fuel slurry **18** may be mixed with oxygen **22** and steam to produce syngas. In particular, the fuel slurry **18** may be reacted with a limited amount of oxygen (e.g., partial oxidation) at elevated pressures (e.g. from absolute pressures of approximately 20 bar to 85 bar) and temperatures (e.g., approximately 700° C. to 1600° C.) to partially oxidize the fuel slurry **18** and produce syngas. Due to chemical reactions between the oxygen **22**, steam, and carbon within the fuel slurry **18**, the syngas may include hydrogen, carbon monoxide, and carbon dioxide, as well as other less desirable components, such as ash, sulfur, nitrogen, and chloride, present in the carbonaceous fuel.

The gasifier **20** may include a reaction portion **24** where partial oxidation may occur and a quench portion **26** where cooling may occur. Within the reaction portion **24**, the fuel slurry **18** may be heated to undergo a pyrolysis process. According to certain embodiments, temperatures inside the gasifier **20** may range from approximately 150° C. to 700° C. during the pyrolysis process, depending on the type of fuel source **12** utilized to generate the fuel slurry **18**. The heating of the feedstock during the pyrolysis process may generate a solid, e.g., char, and residue gases, e.g., carbon monoxide, and hydrogen.

A combustion process may then occur in the gasifier **20**. The combustion may include introducing oxygen to the char and residue gases. The char and residue gases may react with the oxygen to form carbon dioxide and carbon monoxide, which provides heat for the subsequent gasification reactions. According to certain embodiments, temperatures during the combustion process may range from approximately 700° C. to 1600° C. Next, steam may be introduced into the gasifier **20** during a gasification step. The char may react with the carbon dioxide and steam to produce carbon monoxide and hydrogen at temperatures ranging from approximately 800° C. to 1100° C. In essence, the gasifier **20** utilizes steam and oxygen to allow some of the feedstock to be "burned" to produce carbon monoxide and energy, which drives a second reaction that converts further feedstock to hydrogen and additional carbon dioxide. In this way, a resultant gas is manufactured by the gasifier **20**. This resultant gas may include approximately 85% of carbon monoxide and hydrogen, as well as methane, carbon dioxide, water, hydrogen chloride, hydrogen fluoride, carbonyl sulfide, ammonia, hydrogen cyanide, and hydrogen sulfide (depending on the sulfur content of the feedstock). Non-gasifiable ash material and unconverted and/or incompletely converted fuel slurry may be byproducts of the process that may exist as larger particles of molten slag and smaller particles, referred to as fines.

From the reaction portion **24**, the syngas may enter the quench portion **26** where the syngas may be cooled and saturated. The quench portion **26** may be an integral part of the

gasifier **20** as shown, or the quench portion **26** may be a separate unit. The quench portion **26** may cool the syngas to at or near a saturation temperature through evaporation of a cooling fluid, such as water, causing less desirable components to solidify. In particular, the molten slag may be rapidly cooled and solidified into coarse slag particles **28** that may be collected in the bottom of the quench portion **26**.

The coarse slag **28** may flow, for example, by gravity, from the quench portion **26** into a pressurized lock hopper **30** at regular intervals. In certain embodiments, liquid, such as water, may be removed from the coarse slag **28** within the lock hopper **30** and returned to the gasifier **20**. The coarse slag **28** may then be removed from the lock hopper **30** and directed to a slag processing system **34** where the slag **28** may be screened to reduce moisture and then directed to an offsite disposal facility. For example, the slag **28** may be used as road base or as another building material. According to certain embodiments, the slag processing system **34** may include a drag conveyer and/or a slag sump.

In addition to producing slag **28**, the quench portion **26** may produce cooled syngas **36** and black water **38**, which includes fine particles of slag produced by the gasifier **20**. The cooled syngas **36** may be directed to a scrubber **40** where additional fines and other entrained gases, such as hydrogen chloride, may be removed. In particular, within the scrubber **40**, the fines may be separated from the syngas to produce another stream of black water **42** that may exit a bottom portion of the scrubber **40** while scrubbed syngas **44** may exit through an upper portion of the scrubber **40**.

The black water **42** exiting the bottom portion of the scrubber **40** may be combined with the black water **38** from the gasifier **20** and may be directed to a black water processing system **46**. In other embodiments, the black water **38** and the black water **42** may be provided to the black water processing system **46** as separate streams. As described further with respect to FIG. 2, within the black water processing system **46**, the black water **38** and **42** may be subjected to a series of pressure reductions that may cause the black water **38** and **42** to be partially evaporated and cooled to remove dissolved gases and concentrate the fines.

The black water processing system **48** also may include a settling process that produces separated fines **48** and grey water **50**. The separated fines **48** may be recycled to the feed stock preparation system **14** where the fines may be used to provide additional fuel. The grey water **50** may be directed to a grey water treatment system **52** where the grey water **50** may undergo further processing to remove gases, such as ammonia, and solids.

After the additional black water **42** has been removed in the scrubber **40**, the scrubbed syngas **44** may be directed to a syngas cooling and treatment system **54** where the syngas may be further purified to produce sweetened syngas **56**. According to certain embodiments, the syngas cooling and treatment system **54** may include one or more water gas shift reactors that adjust the ratio of hydrogen to carbon monoxide in the scrubbed syngas **44**. Further, the syngas cooling and treatment system **54** may include one or more acid gas removal processes that may remove acid gases, such as hydrogen sulfide, hydrogen chloride, hydrogen fluoride, among others. Further, the syngas cooling and treatment system **54** may include one or more stripping processes for removing ammonia. Moreover, a tail gas treatment process also may be included to remove residual gas components such as ammonia, methanol, or any residual chemicals from upstream processing, such as from a sulfur recovery unit. The sweetened syngas **56** may then be used for a variety of processes such as chemical processing or power generation.

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The syngas cooling and treatment system **54** also may produce liquid **58** that may be used to facilitate deaeration within a deaerator **60**. In particular, a portion **62** of the grey water **50** may be directed to the deaerator **60** to remove oxygen **63** and other dissolved gases that may cause corrosion in downstream components. The deaerator **60** may produce deaerated grey water **64** that may be heated within a heat exchanger **66** and directed to the scrubber **40** as heated grey water **68**. The heat exchanger **66** may transfer heat to the deaerated grey water **64** using vapor **70** from the black water processing system **46**. In particular, the vapor **70** may be directed through the heat exchanger **66** to transfer heat to the deaerated grey water **64** producing cooled vapor **72**. The cooled vapor **72** may be further condensed within a condenser **74** to produce partially condensed vapor **76**. The partially condensed vapor **76** may be directed to a knock out vessel **78** to separate the vapor **80** from liquid components **82**, such as water. The vapor **80** from the knock out vessel **78** may be provided to the syngas cooling and treatment system **54** to assist with certain processes, such as ammonia stripping. The liquid **82** from the knock out vessel **78** may be directed to the deaerator **60** to facilitate deaeration.

FIG. 2 depicts an embodiment of the black water processing system **46** that may employ an ejector. The black water processing system **46** includes four flash tanks **84**, **86**, **88**, and **90**. Although four flash tanks are shown, in other embodiments any number of flash tanks may be employed. Each flash tank **84**, **86**, **88**, and **90** may promote separation of fines through a reduction in pressure that causes the black water to be partially evaporated and cooled, thereby separating dissolved gases from the fines. In particular, each flash tank **84**, **86**, **88**, and **90** may subject the black water **38** and **42** to a progressively lower pressure, thereby facilitating further removal of dissolved gases at each flash tank **84**, **86**, **88**, and **90**. According to certain embodiments, the dissolved gases may include syngas, which may be recovered through the syngas cooling and treatment system **54** (FIG. 1).

The black water **38** and **42** may enter the black water processing system **46** through the high-pressure flash tank **84**. According to certain embodiments, the high-pressure flash tank **84** may operate at a pressure of at least approximately 10 bar. However, in other embodiments, the high-pressure flash tank **84** may operate at any suitable pressure. Within the high-pressure flash tank **84**, the vapor components (e.g., the separated gases) may be discharged as overhead vapor **92** through a top portion while a liquid discharge **94** of black water concentrated with fines may exit through a bottom portion.

The overhead vapor **92** from the high-pressure flash tank **84** may be provided to an ejector **96** to serve as the motive fluid for the ejector **96**. As discussed further below, the ejector **96** may be used to create the vacuums within the vacuum flash tanks **88** and **90**. The liquid discharge **94** from the high-pressure flash tank **84** may enter the low-pressure flash tank **86** where further separation of the vapor and liquid components may occur. In particular, the vapor components may be discharged as overhead vapor **98** through a top portion of the low-pressure flash tank **86** while a liquid discharge **100** of black water concentrated with fines may exit through a bottom portion. In certain embodiments, the overhead vapor **98** may be directed to the deaerator **60** (FIG. 1) to provide heat for the deaeration process. According to certain embodiments, the low-pressure flash tank **86** may operate at a pressure of approximately 2 bar. However, in other embodiments, the low-pressure flash tank **86** may operate as more of an intermediate-pressure flash tank with a pressure of approximately 2 to 10 bar. Moreover, in other embodiments, the

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low-pressure flash tank **86** may operate at any suitable pressure less than the pressure of the high-pressure flash tank **84**.

The liquid discharge **100** from the low-pressure flash tank **86** may enter the first vacuum flash tank **88** where additional separation of the vapor and liquid components may occur. In particular, the vapor components may be discharged as overhead vapor **102** through a top portion of the first vacuum flash tank **88** while a liquid discharge **114** of black water concentrated with fines may exit through a bottom portion. The overhead vapor **102** may be condensed in a condenser **104** to produce at least partially condensed vapor **106** that may be directed to a suction chamber **107** of the ejector **96**.

The first vacuum pressure flash tank **88** also may produce a liquid discharge **108** of black water concentrated with fines that may be directed to the second vacuum flash tank **90** for additional separation of the vapor and liquid components. In particular, the vapor components may be discharged as overhead vapor **110** through a top portion of the second vacuum flash tank **90** while a liquid discharge **114** of black water concentrated with fines may exit through a bottom portion. The overhead vapor **110** may be condensed in a condenser **112** to produce at least partially condensed vapor **113** that may be combined with the partially condensed vapor **106** and directed to the suction chamber **107** of the ejector **96**. However, in other embodiments, the partially condensed vapors **106** and **113** may not be combined prior to entering the ejector **96**. For example, in other embodiments, multiple ejectors **96** may be included and each condensed vapor **106** and **113** may enter a separate ejector **96**.

The liquid discharge **114** from the second vacuum flash tank **90** may be directed through a pump **116** to a settling tank **118**. Within the settling tank **118**, the fines **48** may be separated and provided to the feedstock preparation system **14** for fuel, as described above with respect to FIG. 1. The remaining liquid **120** and any entrained vapor may be directed to a grey water tank **121** for storage of the grey water **50** prior to direction to the grey water treatment system **52** (FIG. 1). In certain embodiments, the grey water tank **121** may include a motive device for circulating suspended particles and also may serve to regulate flow to the grey water treatment system **52**.

As described above, the overhead vapor **92** from the high-pressure flash tank **84** may be used as the motive fluid for the ejector **96**. The ejector **96** is connected through the suction chamber **107** to the vacuum flash tanks **88** and **90**. Within the ejector **96**, the overhead vapor **92** may be discharged through a nozzle **122** as a high velocity jet across the suction chamber **107** to create a vacuum within the vacuum flash tanks **88** and **90**. According to certain embodiments, the vacuum flash tanks **88** and **90** may have an absolute pressure less than approximately 0.5 bar. However, in other embodiments, any suitable pressure may exist in the vacuum flash tanks **88** and **90** where the pressure in vacuum flash tank **90** is less than the pressure in vacuum flash tank **88**. Gases from the vacuum flash tanks **88** and **90** may become entrained in the motive fluid (e.g. the overhead vapor **92** from the high-pressure flash tank **84**) and may be carried through the ejector **96** to a diffuser portion **123** that converts velocity energy into pressure energy. According to certain embodiments, the ejector **96** may include a converging section followed by a diverging section to facilitate conversion of velocity energy into pressure energy. Further, multiple ejectors **96** may be disposed in series, in stages, or in parallel. Moreover, multiple nozzles **122** may be included within an ejector **96** to direct the overhead vapor **92** through the ejector **96**.

Discharge **124** may exit the ejector **96** through the diffuser portion **123**. The discharge **124** may include the overhead

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vapor **92** from the high-pressure flash tank **84** and the entrained vapors **106** and **113** from the vacuum flash tanks **88** and **90**. The discharge **124** may be directed to a knock out vessel **125** to separate the vapor **70** from liquid components **126**. The liquid components **126** may be provided to the grey water tank **121** while the vapor **70** may be discharged overhead and directed to the heat exchanger **66** to heat grey water entering the scrubber **40**, as described above with respect to FIG. 1.

In other embodiments, the number and/or the types of flash tanks **84**, **86**, **88**, and **90** included in the black water processing system **46** may vary. For example, in certain embodiments, three flash tanks (e.g., a high-pressure flash tank, a low-pressure or intermediate-pressure flash tank, and a vacuum flash tank) may be included. In another example, the black water processing system **46** may include a high-pressure flash tank, an intermediate-pressure flash tank, a low-pressure flash tank, and a vacuum flash tank. Further, additional equipment, such as pumps, valves, temperature sensors, and pressure transducers, among others, may be included.

FIG. 3 depicts another embodiment of the black water processing system **46**. Similar to the black water processing system **46** shown in FIG. 2, the black water processing system **46** includes the four flash tanks **84**, **86**, **88**, and **90**. However, rather than using overhead vapor **92** from the high-pressure flash tank **84** as the motive fluid for the ejector **96**, steam **128** from a steam source **130** may be employed as the motive fluid. Steam source **130** may include a steam turbine or other suitable steam source. In the embodiment illustrated in FIG. 3, the vapor **92** from the high-pressure flash tank **84** may represent the vapor **70** shown in FIG. 1 that flows directly to the heat exchanger **66** to heat the grey water, as described above with respect to FIG. 1.

The steam **128** may be discharged as a high velocity jet across the suction chamber **107** connected to the vacuum flash tanks **88** and **90**. The partially condensed vapors **106** and **113** from the vacuum flash tanks **88** and **90** may become entrained in the steam **128**. Accordingly, the discharge **124** may include the steam **128** and the vapors **106** and **113** from the vacuum flash tanks **88** and **90**. The discharge **124** may be directed to the knock out vessel **125** to separate vapor **132** from the liquid components **126**. As discussed above with respect to FIG. 2, the liquid components **126** may be directed to the grey water tank **122**. The vapor **132** may be vented to the atmosphere.

This written description uses examples to disclose the invention, including the best mode, and also to enable any person skilled in the art to practice the invention, including making and using any devices or systems and performing any incorporated methods. The patentable scope of the invention is defined by the claims, and may include other examples that occur to those skilled in the art. Such other examples are intended to be within the scope of the claims if they have structural elements that do not differ from the literal language of the claims, or if they include equivalent structural elements with insubstantial differences from the literal language of the claims.

The invention claimed is:

1. A black water processing system, comprising:

a vacuum pressure flash tank configured to separate gases from black water;

a high-pressure flash tank fluidly coupled to the vacuum pressure flash tank and disposed upstream of the vacuum pressure flash tank; and

an ejector, comprising:

a suction chamber comprising a first inlet and a second inlet;

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wherein the first inlet of the suction chamber is fluidly coupled to the vacuum pressure flash tank, and the second inlet comprises a nozzle fluidly coupled to the high-pressure flash tank and configured to flow a motive fluid from the high-pressure flash tank across the suction chamber to create a vacuum to draw the gases from within the vacuum pressure flash tank, wherein the motive fluid is different from the gases.

2. The black water processing system of claim 1, wherein the motive fluid comprises steam.

3. The black water processing system of claim 1, wherein the high-pressure flash tank is configured to separate the gases from the black water at a pressure greater than a vacuum pressure of the vacuum pressure flash tank.

4. The black water processing system of claim 1, wherein the motive fluid comprises an overhead discharge from the high-pressure flash tank.

5. The black water processing system of claim 1, wherein the ejector comprises only stationary parts.

6. The black water processing system of claim 1, wherein a discharge of the ejector comprises the motive fluid and the separated gases entrained in the motive fluid.

7. The black water processing system of claim 1, comprising an additional vacuum pressure flash tank configured to separate gases from the black water, wherein the suction chamber of the ejector is coupled to the additional vacuum pressure flash tank.

8. A gasification system, comprising:

a high-pressure flash tank configured to separate gases from black water to produce a first discharge of the black water and a second discharge of separated gases;

a vacuum pressure flash tank fluidly coupled to the high-pressure flash tank and disposed downstream of the high-pressure flash tank; and

an ejector comprising a suction chamber, wherein the suction chamber comprises a first inlet and a second inlet, the first inlet is fluidly coupled to the vacuum pressure flash tank, the second inlet is fluidly coupled to the high-pressure flash tank, and a nozzle of the second inlet is configured to discharge the second discharge across the suction chamber to create a vacuum to draw a vapor discharge from the vacuum pressure flash tank through the first inlet of the suction chamber.

9. The gasification system of claim 8, wherein the second discharge comprises an absolute pressure of at least approximately 10 bar.

10. The gasification system of claim 8, wherein the vacuum comprises an absolute pressure less than approximately 0.5 bar.

11. The gasification system of claim 8, comprising a low-pressure flash tank and the vacuum pressure flash tank disposed in series with the high-pressure flash tank, wherein the low-pressure flash tank and the vacuum pressure flash tank are each configured to separate gases from the black water.

12. The black water processing system of claim 8, comprising a gasifier configured to produce a synthetic gas and the black water.

13. A gasification system, comprising:

a gasifier configured to produce a synthetic gas and black water;

a black water processing system fluidly coupled to the gasifier, wherein the black water processing system comprises:

a high-pressure flash tank configured to flash the black water to produce a first vapor discharge of first separated gases and a first liquid discharge of the black water; and



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a vacuum pressure flash tank fluidly coupled to the high-pressure flash tank, wherein the vacuum pressure flash tank is configured to flash the black water to produce a second vapor discharge of second separated gases and a second liquid discharge of the black water; and

an ejector comprising a suction chamber, wherein the suction chamber comprises a first inlet and a second inlet, the first inlet is fluidly coupled to the vacuum pressure flash tank, the second inlet is fluidly coupled to the high-pressure flash tank and a nozzle of the second inlet is configured to discharge the first vapor discharge across the suction chamber to pull the second vapor discharge into the ejector from the vacuum pressure flash tank through the first inlet.

**14.** The gasification system of claim **13**, comprising a condenser configured to condense at least a portion of the second vapor discharge upstream of the ejector.

**15.** The gasification system of claim **13**, comprising a scrubber configured to scrub the synthetic gas to produce additional black water, wherein the high-pressure flash tank is configured to flash the additional black water.

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**16.** The gasification system of claim **15**, comprising a heat exchanger configured to transfer heat from a discharge of the ejector to grey water entering the scrubber.

**17.** The gasification system of claim **13**, wherein the high-pressure flash tank has a first absolute pressure of at least approximately 10 bar and the vacuum pressure flash tank has a second absolute pressure less than approximately 0.5 bar.

**18.** The gasification system of claim **13**, comprising a low-pressure flash tank configured to flash the first liquid discharge to produce a third vapor discharge of third separated gases and a third liquid discharge of the black water, wherein the vacuum pressure flash tank is configured to flash the third liquid discharge.

**19.** The gasification system of claim **13**, comprising an additional vacuum pressure flash tank configured to flash the black water to produce a fourth vapor discharge of fourth separated gases and a fourth liquid discharge of the black water, wherein the suction chamber of the ejector is coupled to the additional vacuum pressure flash tank.

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